

CLAIMS AMENDMENTS

1.-7. (Cancelled)

8. (Currently Amended) Process for α -catalytic fluorination of saturated or olefinic halogenated hydrocarbon(s), the method process comprising

providing a bulk catalyst has a Ni/Cr atomic ratio between 0.02 and 0.4:1 prepared by

(a) impregnating an amorphous chromium III oxide with a solution of a nickel compound, wherein the chromium oxide has a BET specific surface area of greater than 150 m²/g and a pore volume of greater than 0.15 ml/g,

(b) drying the chromium oxide under an inert gas or under air at a temperature of between about 100° C and about 350° C, and

(c) activating the chromium oxide first with HF introduced diluted in air or in an inert gas at a temperature ranging from 150° C and 200° C and then with HF at a temperature less than 400 ° C; and

fluorinating flourination ofthe- saturated or olefinic halogenated hydrocarbon(s) by with HF in a gas phase and in the presence of a-the bulk catalyst-based on chromium and on nickel which are obtained by impregnation of an amorphous chromium III oxide with a solution of a nickel compound,

wherein the chromium oxide used exhibits a BET specific surface area of greater than 150 m²/g and a pore volume of greater than 0.15 ml/g;

wherein the catalyst is dried under an inert gas or under air at a temperature of between 100 and 350° C and then activated with HF,

— wherein HF is first introduced diluted in air or in an inert gas at a temperature ranging from 150 to 200°C and then with pure HF at a temperature of less than 400°C, and
— wherein the Ni/Cr atomic ratio is between 0.02 and 0.4:1.

9. (Canceled).
10. (Canceled).
11. (Currently Amended) Process according to Claim 8, wherein the saturated or olefinic halogenated hydrocarbon(s) is the flourination fluorinated at a temperature is between 50°C and 500°C.
12. (Currently Amended) Process according to Claim 8, wherein the- saturated or olefinic halogenated hydrocarbon(s) is fluorinated for contact fluorination time is between 3 and 100 seconds.
13. (Currently Amended) Process according to Claim 8, wherein the molar ratio: of HF/halogenated hydrocarbon(s) is between 1/1 and 30/1.
14. (Currently Amended) Process according to Claim 8, wherein the flourination of the saturated or olefinic halogenated hydrocarbon(s) is carried out at an absolute pressure of between 0.08 and 2 MPa.
15. (Currently Amended) Process according to Claim 8, wherein the flourination of the saturated or olefinic halogenated hydrocarbon(s) is carried out in the presence of an oxidizing agent.
16. (Currently Amended) Process according to Claim 8, further comprising deactivating wherein the bulk catalyst by, deactivated by coking, ; and is regenerated regenerating the catalyst with a by treatment with air or with oxygen or by a Cl₂/HF mixture, at a temperature of between 250°C and 400°C.

17. (Currently Amended) Process according to Claim 8, wherein the halogenated hydrocarbon(s) is perchloroethylene or 1-chloro-2,2,2-trifluoroethane.

18. (Currently Amended) Process according to Claim 8, wherein the catalyst is activated with pure HF at the temperature between 350°C and 380°C .

19. (Currently Amended) Process according to Claim 11, wherein the fluorination temperature is between 100°C and 450°C .

20. (Currently Amended) Process according to Claim 11, wherein the fluorination temperature is between 120°C and 400°C .

21. (Previously Presented) Process according to Claim 12, wherein the fluorination time is less than 30 seconds.

22. (Currently Amended) Process according to Claim 13, wherein the molar ratio of the HF in the gas phase to /the halogenated hydrocarbon(s)-molar ratio is less than 20/1.

23. (Previously Presented) Process according to Claim 14, wherein the pressure is between 0.1 and 1.5MPa.

24. (Currently Amended) Process according to Claim 15, wherein the oxidizing agent is air or oxygen.